THE SPECIFICATION

On page 1, below the title and before the first paragraph, please insert the following new paragraph:

- - This is a division under 35 USC §120 of U.S. Application Serial No. 09/832,745, filed April 11, 2001, which is a division of Serial No. 09/449,598, filed November 29, 1999, now U.S. Patent No. 6,288,292, which is a continuation of U.S. Application Serial No. 08/533,590, filed September 25, 1995, now U.S. Patent No. 6,034,288, which is a continuation of International Application No. PCT/GB94/00784, filed April 14, 1994. - -

On page 12, amend the paragraph beginning at line 22 as follows:

Referring now to the process illustrated in Figure 4, this process is generally the same as that described with reference to Figure 1 and like components are depicted using the same reference numbering but preceded with the prefix "1". The reactors 110, 112 are interconnected by a conduit 114. The reaction carried out in reactor 112 is effected at a lower temperature than that carried out in reactor 110 and hence some cooling, by cooler 115, is required prior to introduction of the reactants into reactor 112. In addition, by mixing relatively cool trichloroethylene vapour with the hot gaseous stream (typically at a temperature of the order of 330°C) from reactor ~~10~~ 110, the cooling power input

required of the cooler 116 may be reduced. In this aspect of the present invention, instead of vaporising the trichloroethylene prior to mixing it with the hot gaseous product stream from the reactor 110, the trichloroethylene is added to the hot gaseous stream passing through conduit 114 by injecting fluid phase trichoroethylene at a temperature of the order of at least 100°C, typically 100 to 150°C, into the conduit 114. In this way, the trichloroethylene is atomised into droplets by, and thereafter vaporised by, the hot gaseous stream and the relatively colder liquid trichloroethylene assists in cooling the hot gaseous stream prior to entry into the reactor 112. It is preferred to preheat the liquid trichloroethylene prior to introduction into the process gas stream in order to reduce its viscosity and surface tension and thereby aid atomisation, while lowering its density and hence increasing the velocity of the injected stream for a given mass flow rate.

On page 13, amend the paragraph beginning at line 19 to read as follows:

The vaporising unit 120 comprises a Venturi arrangement 122 located by annular housing 124 and support flange 126 clamped between successive conduit sections 114A, B and C within the

conduit section 114A. The Venturi arrangement ~~22~~ 122 comprises an upstream section 128 defining an outwardly flared portion 130 leading to the Venturi throat 132, an intermediate section 134 and a downstream section 136, sections 134 and 136 being of progressively increasing cross-section in the direction of process of gas flow. The upstream section 128 has an outer diameter which is less than the internal diameter of the upstream conduit section 114A so that part of the process gas is diverted from the main flow through annular gap 138 and externally of the upstream section 128. The remaining process gas passes through the Venturi throat 132 and undergoes a pressure drop and accompanying increase in velocity. The annular housing 124 is formed with a number of openings 140 (see Figure 6) through which the process gas can flow and enter the conduit section 114B externally of the sections 134 and 136.